



Thermodynamics

Fundamental Concepts

First Law of Thermodynamics	$\Delta U = Q - W$ <ul style="list-style-type: none"> ΔU: Change in internal energy Q: Heat added to the system W: Work done by the system
Enthalpy (H)	$H = U + PV$ <ul style="list-style-type: none"> U: Internal energy P: Pressure V: Volume
Second Law of Thermodynamics	$\Delta S \geq 0$ (for a closed system) <ul style="list-style-type: none"> ΔS: Change in entropy
Gibbs Free Energy (G)	$G = H - TS$ <ul style="list-style-type: none"> T: Temperature S: Entropy At constant T and P, $\Delta G < 0$ for a spontaneous process.
Helmholtz Free Energy (A)	$A = U - TS$ <ul style="list-style-type: none"> At constant T and V, $\Delta A < 0$ for a spontaneous process.
Heat Capacity	$C_v = (\partial U / \partial T)_v$ $C_p = (\partial H / \partial T)_p$

Equations of State

Ideal Gas Law	$PV = nRT$ <ul style="list-style-type: none"> P: Pressure V: Volume n: Number of moles R: Ideal gas constant T: Temperature
Van der Waals Equation	$(P + a(n/V)^2)(V - nb) = nRT$ <ul style="list-style-type: none"> a, b: Van der Waals constants
Peng-Robinson Equation	$P = (RT)/(V_m - b) - (a\alpha)/(V_m^2 + 2bV_m - b^2)$ <ul style="list-style-type: none"> V_m: Molar volume a, b, α: Peng-Robinson parameters

Thermodynamic Cycles

Carnot Cycle	$\eta = 1 - (T_c/T_h)$ <ul style="list-style-type: none"> η: Efficiency T_c: Cold reservoir temperature T_h: Hot reservoir temperature
Rankine Cycle	Used in steam power plants. Includes pump, boiler, turbine, and condenser.

Fluid Mechanics

Fluid Properties

Density (ρ)	$\rho = m/V$ <ul style="list-style-type: none"> m: Mass V: Volume
Viscosity (μ)	Measure of a fluid's resistance to flow.
Surface Tension (σ)	Energy required to increase the surface area of a liquid.

Fluid Statics

Pressure (P)	$P = F/A$ <ul style="list-style-type: none"> F: Force A: Area
Hydrostatic Pressure	$P = \rho gh$ <ul style="list-style-type: none"> ρ: Density g: Acceleration due to gravity h: Height
Buoyancy	Archimedes' principle: Buoyant force equals the weight of the fluid displaced.

Fluid Dynamics

Continuity Equation	$A_1V_1 = A_2V_2$ (for incompressible fluids) <ul style="list-style-type: none"> A: Cross-sectional area V: Velocity
Bernoulli's Equation	$P + (1/2)\rho V^2 + \rho gh = \text{constant}$ <ul style="list-style-type: none"> P: Pressure ρ: Density V: Velocity g: Acceleration due to gravity h: Height
Navier-Stokes Equations	Equations describing the motion of viscous fluid substances.
Reynolds Number (Re)	$Re = (\rho VD)/\mu$ <ul style="list-style-type: none"> ρ: Density V: Velocity D: Diameter μ: Viscosity
Friction Factor (f)	Used to calculate pressure drop in pipes.

Mass Transfer

Diffusion

Fick's First Law	$J = -D (dC/dx)$ <ul style="list-style-type: none">J: Diffusion fluxD: Diffusion coefficientC: Concentrationx: Distance
Fick's Second Law	$\partial C/\partial t = D (\partial^2 C/\partial x^2)$ <ul style="list-style-type: none">C: Concentrationt: TimeD: Diffusion coefficientx: Distance

Mass Transfer Coefficient

Mass Transfer Coefficient (k)	Relates the mass transfer rate to the concentration difference. $N = k\Delta C$ <ul style="list-style-type: none">N: Mass transfer ratek: Mass transfer coefficientΔC: Concentration difference
--------------------------------------	---

Chemical Reaction Engineering

Reaction Kinetics

Rate Law	$-r_A = k C_A^n$ <ul style="list-style-type: none">$-r_A$: Rate of disappearance of reactant Ak: Rate constantC_A: Concentration of An: Order of reaction
Arrhenius Equation	$k = A \exp(-E_a/RT)$ <ul style="list-style-type: none">k: Rate constantA: Pre-exponential factorE_a: Activation energyR: Gas constantT: Temperature

Distillation

Relative Volatility (α)	$\alpha = (y_A/x_A) / (y_B/x_B)$ <ul style="list-style-type: none">y_A, y_B: Vapor mole fractions of components A and Bx_A, x_B: Liquid mole fractions of components A and B
McCabe-Thiele Method	Graphical method for designing distillation columns.
Fenske Equation	$N_{min} = \log((x_{A,D}/x_{B,D}) * (x_{B,B}/x_{A,B})) / \log(\alpha)$ <ul style="list-style-type: none">N_{min}: Minimum number of trays$x_{A,D}, x_{B,D}$: mole fractions of A and B in distillate$x_{A,B}, x_{B,B}$: mole fractions of A and B in bottoms

Absorption

Stripping Factor (S)	$S = (mG)/L$ <ul style="list-style-type: none">m: Slope of equilibrium lineG: Gas flow rateL: Liquid flow rate
-----------------------------	--

Reactor Types

Batch Reactor	Closed system; reactants are mixed and allowed to react for a certain time.
Continuous Stirred-Tank Reactor (CSTR)	Continuous flow of reactants and products; perfectly mixed.
Plug Flow Reactor (PFR)	Continuous flow; no mixing in the axial direction.

Reactor Design Equations

CSTR Design Equation	$V = (FA_0 X_A) / (-r_A)$ <ul style="list-style-type: none">V: Reactor volumeFA_0: Molar flow rate of A at inletX_A: Conversion of A$-r_A$: Rate of disappearance of A
PFR Design Equation	$V = \int (FA_0 dX_A) / (-r_A)$ <ul style="list-style-type: none">V: Reactor volumeFA_0: Molar flow rate of A at inletX_A: Conversion of A$-r_A$: Rate of disappearance of AIntegration is performed over the range of conversion.